

# Assessment of Corrosive Attack of Fe9Cr1Mo alloys in Pressurised CO<sub>2</sub> for Prediction of Breakaway Oxidation

Supplementary Materials: Derivation of Analytical Solution for Oxidation

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## 1 Description of moving interface position/velocity governed by ‘oxygen’ diffusion field

To appeal to the observed parabolic oxidation kinetics, we introduce an oxygen-containing species in the spinel phase region, with its concentration  $C_O$  governed by:

$$\dot{C}_O = \nabla \cdot (D_O \nabla C_O) \quad (1)$$

where  $D_O$  is the diffusion coefficient, as illustrated in Figure 7 in the main text. The initial concentration in the substrate  $C_O^\circ$ , and boundary concentrations at the magnetite/spinel interface  $C_O^+$  and at the spinel/substrate interface  $C_O^*$  are assumed to be constant.

The velocity of the spinel/substrate interface (relative to the magnetite/spinel interface)  $\mathbf{v}^{+\rightarrow*} = \mathbf{v}^*$  is given by the mass balance at the spinel/substrate interface, consistent with:

$$\mathbf{v}^* (C_O^* - C_O^\circ) = -D_O \nabla C_O^* \quad (2)$$

The observed oxidation kinetics at the protective region shows parabolic behaviour, for simplicity  $D_O$  is assumed compositional-independent, i.e.

$$\dot{C}_O = D_O \nabla^2 C_O \quad (3)$$

For a 1D domain relative to the spinel/magnetite interface (i.e.  $z_x^+ = 0$ ), Equations (2) and (3) have the following explicit solution by using the similarity method (which is detailed in the next two sections),

$$z_x^* \{t\} = \beta \sqrt{D_O t + (z_x^{*,\circ} / \beta)^2} \quad (4)$$

where  $z_x^{*,\circ}$  is the initial thickness of the spinel phase region at  $t = 0$ ; the parameter  $\beta$  is defined implicitly as the solution of Equation (5):

$$\sqrt{\pi} \beta (C_O^* - C_O^\circ) \operatorname{erf} \{\beta/2\} = 2 (C_O^+ - C_O^*) \exp \{-\beta^2/4\} \quad (5)$$

Here superscripts  $+$ ,  $*$ ,  $\diamond$  and  $\times$  denote interfaces of magnetite/spinel, spinel/substrate, gas/substrate and gas/magnetite, respectively.

## 2 System of equations

For a 1D domain with a fixed left boundary and a moving right boundary, satisfying:

$$\begin{aligned}\dot{C} &= \nabla \cdot (D_O \nabla C) \\ C &= C_0 \quad \text{when } t = 0, \\ C &= C_{\max} \quad \text{at } z_x = 0, \\ C &= C_{\min} \quad \text{at } z_x = X\{t\},\end{aligned}\tag{6}$$

where  $C_{\max}$ ,  $C_{\min}$ ,  $D_O$  and  $C_0$  are constants;  $X\{t\}$  is the position of the moving interface, with its velocity governed by the mass balance at the interface consistent with:

$$\dot{X}\{t\}(C_{\min} - C^*) = -D_O \frac{dC}{dz_x}\tag{7}$$

where  $C^*$  is the concentration at the right-hand side of the moving interface  $X\{t\}$ .

The initial size of the moving domain is  $X_0$ , i.e.  $X\{0\} = X_0$  where  $X_0$  is a constant.

See illustration in Figure 1 for definitions.

## 3 Analytical solution by using the similarity method

We modify the well-known similarity method (e.g. Crank [1]) to treat a moving oxidation region in which we have boundary conditions given in Equation (6) at both  $z_x = 0$  and on a moving boundary  $X\{t\}$ . Since in this case we have an initial region  $X\{0\} = X_0$  we use the transformation given in Equation (8) below to transform the partial differential equation to an ordinary one.

The time shift  $t_0$  is chosen to satisfy the condition  $X\{0\} = X_0$ . For consistency, the derived solution requires that the concentration profile for  $0 < z_x < X_0$  satisfies Equation (17).

Defining:

$$\eta = \frac{z_x}{\sqrt{D_O(t + t_0)}}\tag{8}$$

we can convert the governing PDE to an ODE:

$$F''\{\eta\} + \frac{\eta}{2}F'\{\eta\} = 0\tag{9}$$

where  $C = F\{\eta\}$ .

Solving Equation (9), we have:

$$F\{\eta\} = c_2 + c_1 \cdot \sqrt{\pi} \cdot \operatorname{erf}\{\eta/2\} \quad (10)$$

We also have the boundary condition:

$$\eta = 0 \quad \text{when } F = C_{\max} \quad (11)$$

$$\eta = \beta \quad \text{when } F = C_{\min} \quad (12)$$

where  $X\{t\} = \beta\sqrt{D_O(t+t_0)}$ , is the assumed expression for the moving domain required for the solution of the ordinary Equation (9).

This gives:

$$F\{\eta\} = C_{\max} + \frac{(C_{\min} - C_{\max})\operatorname{erf}\{\eta/2\}}{\operatorname{erf}\{\beta/2\}} \quad (13)$$

and

$$F'\{\eta\} = \frac{(C_{\min} - C_{\max})\exp\{-\eta^2/4\}}{\sqrt{\pi} \cdot \operatorname{erf}\{\beta/2\}} \quad (14)$$

We can also transform the mass balance Equation (7) as:

$$\frac{\beta}{2}(C_{\min} - C^*) = -F'\{\beta\} \quad (15)$$

Equations (14) and (15) give  $\beta \approx 1.2401$ , if  $C_{\min} = 0.5$ ,  $C_{\max} = 1$  and  $C^* = 0$ .

$t_0$  is obtained from the condition  $X\{0\} = X_0$  as:

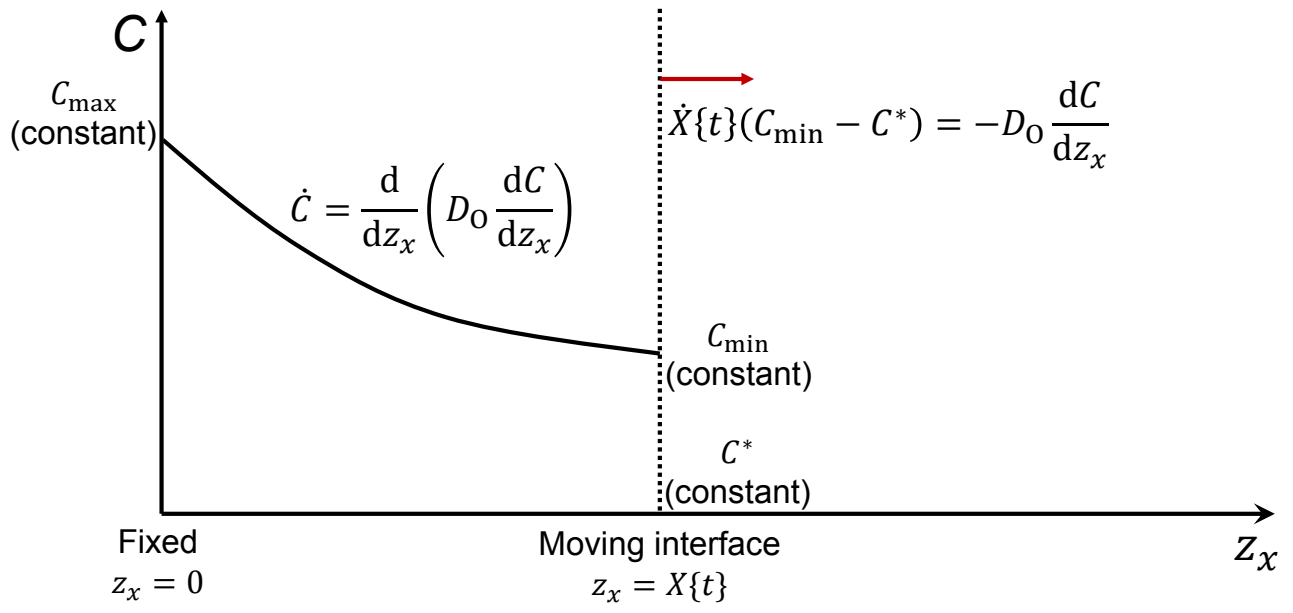
$$t_0 = \frac{X_0^2}{\beta^2 D_O} \quad (16)$$

Initial concentration profile following Equation (17) in 1D (i.e.  $t = 0$  of Equation (13)) should give the initial steady state.

$$C\{z_x\} = C_{\max} + \frac{(C_{\min} - C_{\max})}{\operatorname{erf}\{\beta/2\}} \operatorname{erf}\left\{\frac{\beta z_x}{2X_0}\right\} \quad (17)$$

## References

- [1] J. Crank, The mathematics of diffusion, Oxford University Press, 1975.



**Figure 1:** Definitions for solving the moving interface problem.